LISTING OF THE CLAIMS:

Claim 1 (Currently Amended): A process for the production of food-grade phosphoric acid by the crystallization of phosphoric acid hemihydrate, H₃PO₄ x 0.5 H₂O, from a prepurified feed acid, wherein the feed acid used for the crystallization is purified by the following steps comprising:

purifying the feed acid used for crystallization by the following steps a, b and c:

- a) after the <u>a</u> froth-flotation step of <u>a</u> phosphate concentrate, the concentrate is directed to a strongly magnetic separation step for the decreasing of the <u>an</u> Mg ion amount,
- b) the phosphate concentrate is leached in a mixture of sulfuric acid and phosphoric acid according to the \underline{a} wet process, the precipitated SO_4 and As ions are removed, and a source of silicon is added in order to adjust the \underline{an} F/Si molar ratio to < 6,
- c) the phosphoric acid is concentrated, the <u>a</u> solids precipitate is removed and the F ions are evaporated, <u>and</u>
- d) the feed acid obtained from step c, having a concentration of $> 58 \text{ wt.}\% \text{ P}_2\text{O}_5$, a solids concentration of < 0.05 wt.%, an Mg ion concentration of < 1.5 wt.%, an SO₄ ion concentration of < 1 wt.%, an As ion concentration of < 8 ppm, and an F ion concentration of < 0.2 wt.%, is crystallized at a steady crystal growth rate of < 10 µm/min, corresponding to < 25 wt.% crystals/hour, when seed crystals are added in an amount of at maximum 2 wt.% in the form of a 40 wt.% crystal slurry, in which the an Fe ion concentration is < 500 ppm and seed crystal size is < 200 µm, the temperature difference being in the a first crystallization being < 17 °C, and the crystals are washed with the an undersaturated mother liquor of the a subsequent recrystallization step,
- e) the phosphoric acid crystallized in step d is melted, diluted to a concentration of < 63 wt.% P_2O_5 , seed crystals are added, and crystallization is carried out as in step d, the

temperature difference being < 8 °C, and the crystals are washed with an undersaturated solution of phosphoric acid, and

f) optionally the phosphoric acid crystallized in step e is melted, diluted to a concentration of $< 63 \text{ wt.}\% \text{ P}_2\text{O}_5$, seed crystals are added, and crystallization is carried out as in step d, the temperature difference being < 6 °C, and the crystals are washed with an undersaturated washing solution prepared from product crystals.

Claim 2 (Previously Presented): A process according to Claim 1, wherein the process comprises one recrystallization step e.

Claim 3 (Previously Presented): A process according to Claim 1, wherein the process comprises two recrystallization steps e and f, the crystals of step e being washed with an undersaturated mother liquor obtained from the subsequent recrystallization step f.

Claim 4 (Previously Presented): A process according to Claim 1, wherein the mother liquor of the first crystallization step d is separated as a fodder-grade phosphoric acid.

Claim 5 (Previously Presented): A process according to Claim 1, wherein the acid crystallized in steps e and/or f is melted and diluted to food-grade phosphoric acid.

Claim 6 (Previously Presented): A process according to Claim 1, wherein the crystallization step of the process is implemented as a batch process or a continuous-working process.

Claim 7 (Previously Presented): A process according to Claim 1, wherein the mother liquors of recrystallization steps e and/or f are recycled as feed acid to the same and/or preceding step.

Claim 8 (Currently Amended) A process according to Claim 1, wherein a magnetic flux density of at minimum 1 Tesla, preferably 1-3 Tesla, is used in step a.

Claim 9 (Previously Presented): A process according to Claim 1, wherein in the crystallization steps of the process the viscosity of the crystal slurry is < 2000 cP.

Claim 10 (Currently Amended) A process according to Claim 1, wherein in crystallization step d the concentration of the feed acid is $< 61 \text{ wt.}\% \text{ P}_2\text{O}_5$, the Mg ion concentration is < 1.2 wt.% Mg, and the F ion concentration is < 0.18 wt.%.

Claim 11 (New) A process according to claim 8, wherein a magnetic flux density of 1-3 Tesla is used in step a.